

A New Type of Strong Metal–Support Interaction and the Production of H₂ through the Transformation of Water on Pt/CeO₂(111) and Pt/CeO_x/TiO₂(110) Catalysts

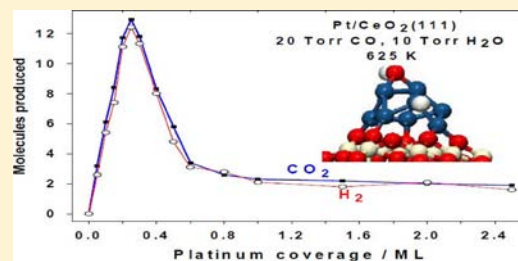
Albert Bruix,[†] José A. Rodríguez,^{*,‡} Pedro J. Ramírez,[§] Sanjaya D. Senanayake,[‡] Jaime Evans,[§] Joon B. Park,[‡] Dario Stacchiola,[‡] Ping Liu,[‡] Jan Hrbek,[‡] and Francesc Illas[†]

[†]Departament de Química Física and Institut de Química Teòrica i Computacional (IQTCUB), Universitat de Barcelona, Martí i Franques 1, 08028 Barcelona, Spain

[‡]Chemistry Department, Brookhaven National Laboratory, Upton, New York 11973, United States

[§]Facultad de Ciencias, Universidad Central de Venezuela, Caracas 1020-A, Venezuela

ABSTRACT: The electronic properties of Pt nanoparticles deposited on CeO₂(111) and CeO_x/TiO₂(110) model catalysts have been examined using valence photoemission experiments and density functional theory (DFT) calculations. The valence photoemission and DFT results point to a new type of “strong metal–support interaction” that produces large electronic perturbations for small Pt particles in contact with ceria and significantly enhances the ability of the admetal to dissociate the O–H bonds in water. When going from Pt(111) to Pt₈/CeO₂(111), the dissociation of water becomes a very exothermic process. The ceria-supported Pt₈ appears as a fluxional system that can change geometry and charge distribution to accommodate adsorbates better. In comparison with other water-gas shift (WGS) catalysts [Cu(111), Pt(111), Cu/CeO₂(111), and Au/CeO₂(111)], the Pt/CeO₂(111) surface has the unique property that the admetal is able to dissociate water in an efficient way. Furthermore, for the codeposition of Pt and CeO_x nanoparticles on TiO₂(110), we have found a transfer of O from the ceria to Pt that opens new paths for the WGS process and makes the mixed-metal oxide an extremely active catalyst for the production of hydrogen.



INTRODUCTION

Metal–oxide interfaces play a key role in a large set of technologically important applications such as metal–oxide contacts in microelectronics and photovoltaic devices, gas sensors, coatings for electrochemical devices or corrosion passivation, and oxide-supported transition-metal catalysts.¹ Over the years, a large number of studies have been focused on improving our understanding of the atomic-level structure of metal–oxide interfaces, the electronic character of the metal atoms that are right at these interfaces, and the energetics of bonding and thermodynamic stability of these interfaces.^{1,2} These are critical issues connected to technological applications. In a classic article, Tauster et al.^{3a} used the term “strong metal–support interaction” to describe the drastic changes that occur in the chemisorption properties of Pt and other group VIII (8–10) metals when they are dispersed on surfaces of titanium oxide. The ability to chemisorb H₂ or CO was strongly suppressed or vanished entirely when these metals were supported on TiO₂ and activated in H₂ at elevated temperatures.³ A strong metal–support interaction had somehow deprived these metals of one of their most characteristic chemical properties, making them catalytically inactive.³ The spreading of TiO_x aggregates on the surface of the supported metals could be responsible for the reduction in their chemical and catalytic activity.^{3b,4} In this article, we report a completely

different type of strong metal–support interaction that *substantially enhances* the catalytic activity of Pt for the generation of hydrogen through the water-gas shift (WGS) reaction, CO + H₂O → H₂ + CO₂.

In industry, the WGS reaction is widely used to produce the hydrogen necessary for many chemical processes⁵ and to eliminate the CO present in feed streams for ammonia synthesis and fuel cells.⁶ There is a continuous search for new and more efficient WGS catalysts.^{6,7} Supported platinum catalysts have received much interest during the past decade because of their WGS activity at low temperatures.^{6–14} The WGS has been investigated over Pt nanoparticles (NPs) dispersed over various oxide supports: Al₂O₃, CeO₂, ZrO₂, CeO₂/ZrO₂, and TiO₂.^{7–14} Among the oxide supports, the CeO₂ and TiO₂ substrates are two of the most promising candidates for the WGS process. The reason that the nature of the oxide is important for the good performance of Pt-based catalysts is a matter of debate.^{6–14} Furthermore, a recent study of the WGS on Pt(111) indicates that there can be problems in performing the reaction on extended surfaces of platinum.¹⁵ The turnover frequency of Pt(111) is initially 5 times greater than that observed on Cu(111), a typical benchmark for the

Received: March 1, 2012

Published: May 7, 2012

WGS reaction,^{16–18} but Pt(111) undergoes deactivation due to the deposition of carbon by the Boudouard reaction: $2\text{CO}(\text{surf}) \rightarrow \text{C}(\text{surf}) + \text{CO}_2(\text{g})$.¹⁵ Thus, why is Pt/CeO₂ a very good catalyst for the WGS reaction? In this work, we used experiment and theory to investigate the WGS reaction on well-defined Pt/CeO₂(111) surfaces and to explain the high performance of the admetal in Pt/CeO₂ catalysts. The results of valence photoemission experiments and density functional theory (DFT) calculations point to a new type of strong metal–support interaction that produces large electronic perturbations for small Pt particles in contact with CeO₂(111) and significantly enhances the ability of the admetal to dissociate the O–H bonds in water. Upon going from Pt(111) to Pt₈/CeO₂(111), the dissociation of water becomes a very exothermic process. Furthermore, for the codeposition of Pt and CeO_x NPs on TiO₂(110), we have found a transfer of O from the ceria to Pt that opens new paths for the WGS process and makes the mixed-metal oxide an extremely active catalyst for the production of hydrogen.

EXPERIMENTAL AND THEORETICAL METHODS

The photoemission and catalytic studies were carried out in a system combining an ultrahigh-vacuum (UHV) chamber (base pressure $\sim 5 \times 10^{-10}$ Torr) and a batch reactor.^{18–20} The sample could be transferred between the reactor and the UHV chamber without exposure to air. The UHV chamber (base pressure $\sim 5 \times 10^{-10}$ Torr) was equipped with instrumentation for X-ray and UV photoelectron spectroscopies (XPS and UPS), low-energy electron diffraction (LEED), ion scattering spectroscopy (ISS), and temperature-programmed desorption (TPD). The microscopy studies were carried out in an Omicron variable-temperature scanning tunneling microscopy (STM) system directly attached to a main UHV chamber equipped with optics for LEED, instrumentation for Auger electron spectroscopy, and surface cleaning facilities. The kinetic tests were done using CeO₂(111) and TiO₂(110) single crystals cleaned following standard procedures used in our previous studies of Au/CeO₂(111) and Au/TiO₂(110).^{19,20} To avoid problems with charging in the XPS and UPS experiments, films of CeO₂(111) were grown in situ onto a Ru(0001) substrate (700 K) using a four-pocket Oxford evaporator in an O₂ atmosphere (1×10^{-7} Torr). Previous studies have been devoted to understanding this growth and the formation of well-defined (111) surfaces.^{21,22} The Oxford evaporator was also used to deposit CeO_x on TiO₂(110).^{20,23} Pt was evaporated onto CeO₂(111) and CeO_x/TiO₂(110) at 300 K. In the kinetic measurements, the sample was transferred to the batch reactor at ~ 300 K, after which the reactant gases were introduced (20 Torr CO and 10 Torr H₂O) and the sample was rapidly heated to the reaction temperature of 625 K. The number of molecules produced was normalized to the active area exposed by the sample.^{19,20} In our reactor, a steady-state regime for the production of H₂ and CO₂ was reached after 2–3 min of reaction time.

The DFT calculations were performed using the VASP program (version 4.6)²⁴ and the methodology described in refs 25 and 26. We used the PW91 exchange–correlation functional, and the description of stoichiometric and reduced ceria was achieved within the so-called GGA+U approach with a *U* value of 4 eV.^{27,28} The kinetic energy cutoff was 415 eV.²⁴ The Pt₈/CeO₂(111) calculations employed a slab of three CeO₂ (nine atomic) layers and a 3×4 surface cell. The space between neighboring slab images was 1.5 nm.²⁴ Complete geometry optimizations were carried out for NP models, and only atoms in the bottom O–Ce–O layer were kept fixed at the bulk positions during the local-minimum search in the slab calculations.

RESULTS AND DISCUSSION

We start by examining the catalytic properties of Pt on CeO₂(111). Since Pt/CeO₂ powder catalysts typically have small loadings of the noble metal (< 2 wt %),⁶ we are

particularly interested in low coverages of Pt on CeO₂(111). STM has been used to study the growth mode of Pt on CeO₂(111) films supported on Ru(0001).²⁹ Deposition of 0.2 monolayer (ML) of Pt on CeO₂(111) at 300 K produces small metal NPs on the ceria terraces with a height of two atomic layers. The introduction of oxygen vacancies in the oxide surface to give CeO_{1.88}(111) leads to a better dispersion of the Pt, and the small metal aggregates now exhibit a height of one or two atomic layers.²⁹ Using XPS and He-II UPS, we investigated the interaction of Pt with the CeO₂(111) crystal. After depositing 0.1–0.2 ML of Pt on CeO₂(111), we measured Pt 4f_{7/2} core-level binding energies that were 0.7–0.9 eV higher than that found for bulk metallic Pt (71.2 eV). At the same time, UPS spectra for the valence region of the Pt/CeO₂(111) systems (Figure 1) exhibited a density of Pt 5d

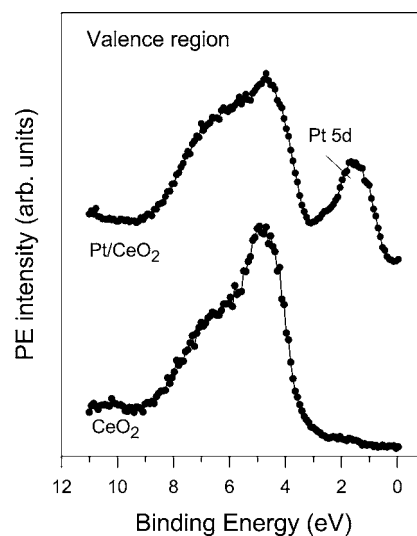


Figure 1. He-II valence UPS spectra collected before and after deposition of 0.15 ML of Pt on a CeO₂(111) surface.

states near the Fermi level that was much smaller than that expected for metallic Pt.³⁰ In the case of Pt(111), a strong photoemission signal was observed between 0 and 1 eV,³⁰ whereas for Pt/CeO₂(111) ($\theta_{\text{Pt}} < 0.25$ ML), there was a weak signal in this region. Small metal particles can exhibit a reduced density of d states near the Fermi edge when deposited on oxides.¹ Our results of photoelectron spectroscopy are consistent with previous experimental and theoretical studies that point to a Pt → ceria charge transfer when small particles of Pt are in contact with CeO₂(111).^{25,26} As we will show below, the perturbations in the electronic properties of the supported Pt NPs lead to an important change in their chemical properties.

Figure 2 displays the WGS activities of a large series of model Pt/CeO₂(111) catalysts. The clean CeO₂(111) surface did not have activity for the WGS reaction under the reaction conditions investigated here. Upon addition of Pt to CeO₂(111), there was a continuous increase in the catalytic activity until a maximum was reached at a coverage of ~ 0.2 ML. After this point, the production of H₂ and CO₂ decreased drastically as the Pt coverage was raised. Postreaction surface characterization with XPS indicated that during the WGS process the ceria support was partially reduced, reaching a composition of CeO_{1.90–1.93}. Comparing these data with the STM results reported for the Pt/CeO₂(111) and Pt/

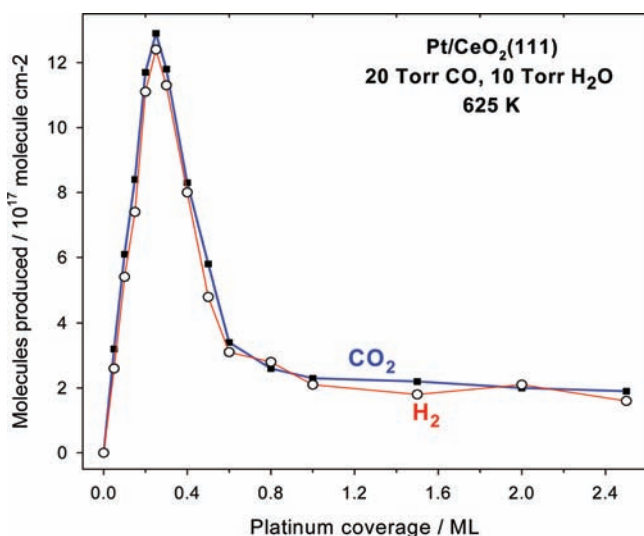


Figure 2. WGS activities of model Pt/CeO₂(111) catalysts as a function of admetal coverage. Each surface was exposed to a mixture of 20 Torr CO and 10 Torr H₂O at 625 K for 5 min.

CeO_{1.88}(111) systems,²⁹ one can conclude that the maximum activity in Figure 2 corresponds to catalysts that contain Pt particles with a diameter smaller than 1.7 nm and a height less than 0.4 nm. Furthermore, the measured catalytic activity is correlated with the magnitude of the electronic perturbations seen in UPS. The Pt/CeO₂(111) catalysts with the highest activity ($\theta_{\text{Pt}} < 0.3$ ML) displayed a lower density of Pt 5d states near the Fermi level (Figure 1), while the catalysts with lower activity ($\theta_{\text{Pt}} > 0.8$ ML) exhibited a density of Pt 5d states near the Fermi level that was not much different from that of bulk metallic Pt(111).³⁰

In test experiments, we found no signs of deactivation of the Pt/CeO₂(111) ($\theta_{\text{Pt}} < 0.3$ ML) catalysts after 2 h of reaction time. In the case of the WGS reaction on Pt(111), deactivation by deposition of carbon is observed after reaction times of 10–20 min.¹⁵ Using plots for H₂ production versus time (Figure 3), we calculated the corresponding reaction rates and turnover numbers for the WGS reaction on Pt/CeO₂(111). Assuming

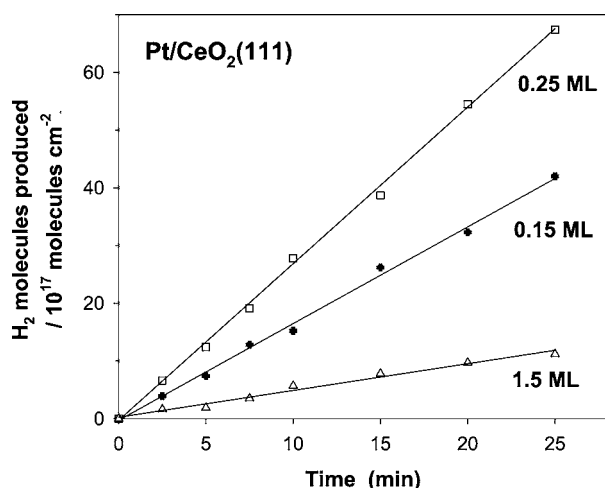


Figure 3. Numbers of H₂ molecules produced via the WGS reaction as functions of time on Pt/CeO₂(111) catalysts containing 0.15, 0.25, and 1.5 ML of Pt. Each surface was exposed to a mixture of 20 Torr CO and 10 Torr H₂O at 625 K.

that all of the Pt atoms deposited on CeO₂(111) participated in the reaction, we estimated turnover frequencies of 12.4 ($\theta_{\text{Pt}} = 0.15$ ML) and 11.5 ($\theta_{\text{Pt}} = 0.25$ ML) molecules Pt_{site}⁻¹ s⁻¹ for the highly active catalysts in Figure 2. These are *much larger* than the value of 0.53 molecules Pt_{site}⁻¹ s⁻¹ reported for Pt(111).¹⁵ A comparison of the performance of Pt/CeO₂(111) with those of catalysts containing Ni,³¹ Cu,²⁰ or Au²⁰ dispersed on CeO₂(111) (Figure 4) indicates that the Pt-based system is

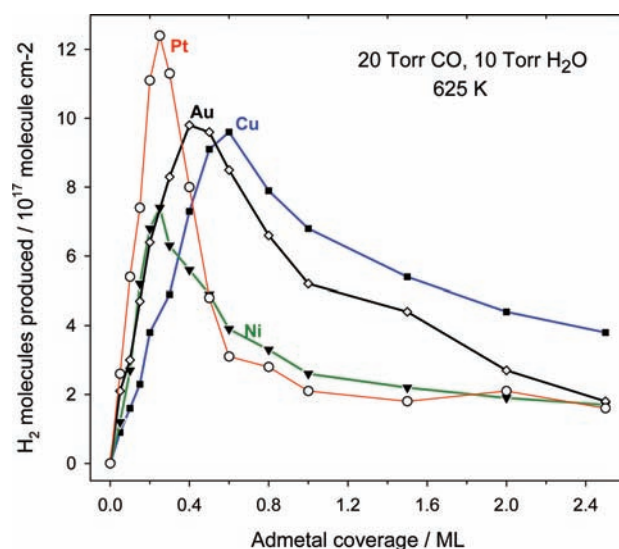
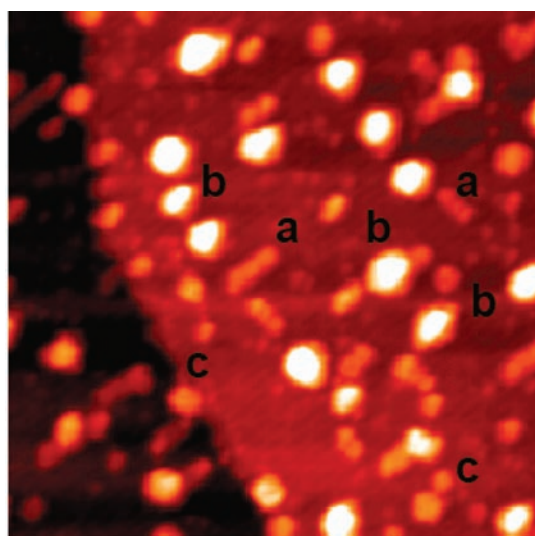


Figure 4. Numbers of H₂ molecules produced via the WGS reaction on catalysts generated by deposition of Pt (this work), Ni (ref 31), Cu (ref 20), and Au (ref 20) on CeO₂(111). Each surface was exposed to a mixture of 20 Torr CO and 10 Torr H₂O at 625 K for 5 min.

clearly the best in terms of activity and low loading of the admetal under the conditions investigated in these studies (20 Torr CO and 10 Torr H₂O at 625 K). Systems such as Au/CeO₂(111) and Cu/CeO₂(111) exhibit better performance than Pt/CeO₂(111) only at large loadings of the admetal (>0.3 ML), where the Pt catalytic activity substantially decreases, probably as a result of the fact that most of the Pt atoms are not in contact with the ceria support. A look at data reported in the literature for the performance of high-surface-area catalysts during the WGS reaction under various conditions also indicated that Pt/CeO₂ shows excellent activity.⁶

To enhance the interactions between Pt and ceria, we coadsorbed NPs of both on a TiO₂(110) substrate. The properties of the CeO_x/TiO₂(110) mixed metal oxide have been examined using STM and core and valence photoemission.^{19,23} At small coverages, ceria deposited on TiO₂(110) forms short wirelike nanostructures that contain dimers of Ce₂O₃ and exhibit a characteristic height of 1.4 ± 0.2 Å in STM.¹⁹ On the other hand, the deposition of small coverages of Pt on clean TiO₂(110) produces round particles with heights of 3–6 Å,³² which is considerably larger than the height of the Ce₂O₃ dimers in CeO_x/TiO₂(110).¹⁹ From an analysis of the shape and height of the features in the STM image of Pt/CeO_x/TiO₂(110) (Figure 5), one can identify three types of structures. The surface contains NPs of CeO_x with a wirelike structure and a height close to 1.4 Å (labeled as “a”). On top of or near the ceria structures, there are bright features with heights of 4–9 Å that correspond to Pt particles in direct contact with ceria (labeled as “b”). Finally, there are small round features that have heights of 3–5 Å that were not seen in



30 nm x 30 nm

Figure 5. STM image taken after deposition of ~ 0.15 ML of Pt on a $\text{CeO}_x/\text{TiO}_2(110)$ surface. The deposition of Pt was done at 300 K, with subsequent heating to 625 K. The surface contains NPs of CeO_x with a wire-like structure (a), Pt particles on top of ceria (b, bright dots), and Pt particles on top of TiO_2 (c). Conditions: $V_t = 1.2$ V; $I_t = 0.05$ nA.

STM images of $\text{CeO}_x/\text{TiO}_2(110)$ ¹⁹ and probably correspond to Pt particles on top of the $\text{TiO}_2(110)$ substrate (labeled as “c”).³² When the CeO_x coverage on $\text{TiO}_2(110)$ was raised, STM showed the coalescence of the wirelike ceria nanostructures and the formation of three-dimensional islands.²³ In general, our STM results indicate that these ceria islands can act as excellent nucleation centers for the growth of Pt particles. Thus, in $\text{Pt}/\text{CeO}_x/\text{TiO}_2(110)$, there is close contact between Pt and ceria.

Ce 3d XPS data indicated Ce to be mainly in the +3 oxidation state in the $\text{CeO}_x/\text{TiO}_2(110)$ and $\text{Pt}/\text{CeO}_x/\text{TiO}_2(110)$ systems. Figure 6 shows Ce 3d XPS spectra collected after deposition of 0.1, 0.25, or 0.5 ML of ceria on $\text{TiO}_2(110)$. Similar line shapes were found after the deposition of Pt on the generated $\text{CeO}_x/\text{TiO}_2(110)$ surfaces. The line shapes shown in Figure 6 point to Ce^{3+} as the dominant cation species in the supported ceria.³³ The Ce 3d line shape for Ce^{4+} in stoichiometric CeO_2 is quite different.³³ UPS spectra taken after deposition of small amounts of Pt (0.1–0.2 ML) on $\text{CeO}_x/\text{TiO}_2(110)$ again showed a weak density of Pt 5d states near the Fermi level, as seen in the case of $\text{Pt}/\text{CeO}_2(111)$, indicating the existence of electronic perturbations in the admetal. The Pt 4f XPS spectra of $\text{Pt}/\text{CeO}_x/\text{TiO}_2(110)$ (Figure 7) exhibited a line shape with an apparent inversion of the usual ratio of intensities expected for the $5/2$ and $7/2$ peaks of metallic platinum.³⁴ This phenomenon has been seen before for the interaction of oxygen with platinum surfaces and is consistent with the presence of some O on the supported Pt NPs.³⁴ This is in agreement with recent results for Pt on nanostructured ceria showing a migration of O from the ceria to Pt that is not seen in the case of Pt deposited on a bulk $\text{CeO}_2(111)$ surface.²⁶

Figure 8 shows the WGS activity of $\text{Pt}/\text{TiO}_2(110)$ and two sets of $\text{Pt}/\text{CeO}_x/\text{TiO}_2(110)$ catalysts in which 11 or 23% of the titania substrate was covered by ceria particles. The fraction of the titania covered by ceria was measured using ISS¹⁹ before deposition of the Pt. The maximum activities were seen for

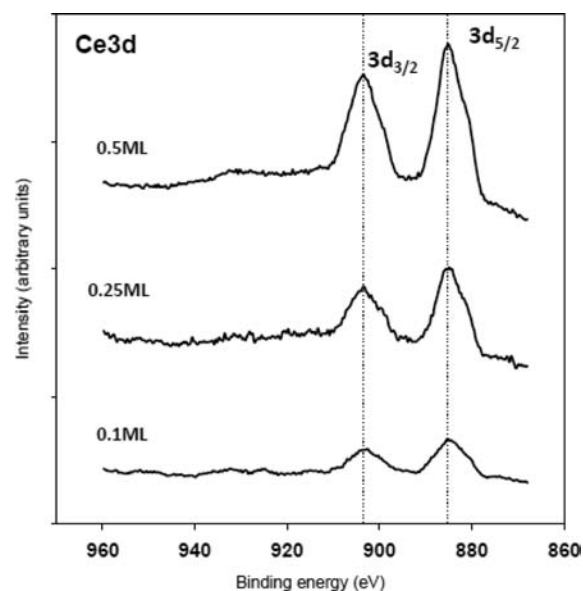


Figure 6. Ce 3d XPS spectra collected after deposition of 0.1, 0.25, or 0.5 ML of ceria on $\text{TiO}_2(110)$. Similar line shapes were found after the deposition of Pt.

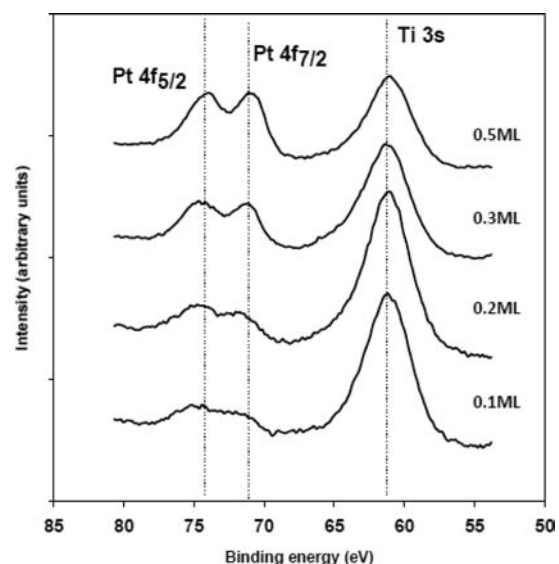


Figure 7. Pt 4f photoemission spectra collected after deposition of different coverages of Pt (0.1, 0.2, 0.3, or 0.5 ML) on a titania surface precovered with 0.2 ML of ceria. The unusual ratio of the intensities of the $5/2$ and $7/2$ peaks in the Pt 4f region points to the presence of some O on top of the Pt.³⁴

catalysts containing a small amount of Pt ($\theta_{\text{Pt}} < 0.3$ ML) and ceria (11% of the titania covered). These systems did not show signs of deactivation with time after kinetic tests of up to 2 h. The estimated turnover frequencies for catalysts containing 0.15 ML of Pt were 34.8 (11% of titania covered by ceria) and 28.6 (23% of titania covered by ceria) molecules $\text{Pt}_{\text{site}}^{-1} \text{s}^{-1}$. For this small Pt coverage, the $\text{Pt}/\text{CeO}_x/\text{TiO}_2(110)$ catalysts were 2.3–2.8 times more active than the corresponding $\text{Pt}/\text{CeO}_2(111)$ catalyst. On the other hand, at large coverages of Pt (> 0.8 ML), when most of the metal adatoms are not affected by interactions with ceria and the Pt exhibits a large density of 5d states near the Fermi level, the catalytic activities of the Pt/

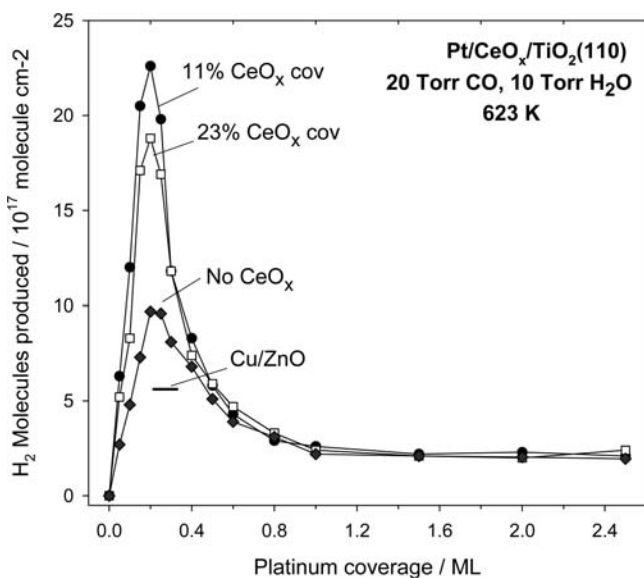


Figure 8. WGS activities of model Pt/TiO₂(110) and Pt/CeO_x/TiO₂(110) catalysts as functions of admetal coverage. Before vapor deposition of the Pt, ceria was dispersed on TiO₂(110) covering 11 and 23% of this substrate. Each surface was exposed to a mixture of 20 Torr CO and 10 Torr H₂O at 625 K for 5 min. For comparison, we have included the maximum activity found for the WGS reaction on the Cu/ZnO(000 $\bar{1}$) system ($\theta_{\text{Cu}} = 0.5$ ML).²⁰

CeO_x/TiO₂(110) and Pt/CeO₂(111) systems are very close and similar to that of bulk Pt.

Cu/ZnO catalysts are frequently used in industrial processes for the production of hydrogen via the WGS reaction.^{5,6} Pt/CeO_x/TiO₂ exhibits a WGS activity substantially higher than those of Cu/ZnO(000 $\bar{1}$)²⁰ and Pt/TiO₂, Pt/CeO₂, and clean Pt(111).¹⁵ Pt gets activated by electronic interactions with ceria, and these Pt \leftrightarrow CeO_x interactions seem to be stronger when one has small platinum and ceria NPs. The dissociation of water is frequently the rate-determining step for the WGS reaction on metal or metal/oxide surfaces.^{6,16–18} In TPD experiments, we found that the Pt/CeO_x/TiO₂(110) surfaces were able to dissociate water *all the way* to yield molecular H₂. Figure 9 displays TPD spectra acquired after dosing water onto the catalyst with the highest activity in Figure 8 ($\theta_{\text{Pt}} = 0.2$ ML, 11% of the titania covered by CeO_x). None of the features seen in Figure 9 was observed in control experiments when water was not dosed onto the Pt/CeO_x/TiO₂(110) surface. The strong H₂O peak near 180 K matches desorption temperatures found for water on TiO₂(110), CeO₂(111), and Pt(111).^{35,36} The H₂O desorption features seen between 200 and 350 K were also observed after the molecule was dosed onto plain CeO_x/TiO₂(110). On the other hand, the H₂ desorption peak from 400 to 500 K and the O₂ desorption features between 550 and 700 K are *all unique* to the Pt/CeO_x/TiO₂(110) system and come from the full decomposition of water on the supported Pt NPs.

Our DFT calculations also point to facile dissociation of water on small Pt clusters electronically perturbed by interactions with ceria. We investigated the dissociation of water on Pt(111), on free Pt₇₉ and Pt₈ particles,^{25,26} and at Pt₈–ceria interfaces (see the corresponding structures in Figure 10). These systems were chosen taking into consideration previous studies showing that the activities of very small metal clusters supported on SiO₂ and MgO are very different from

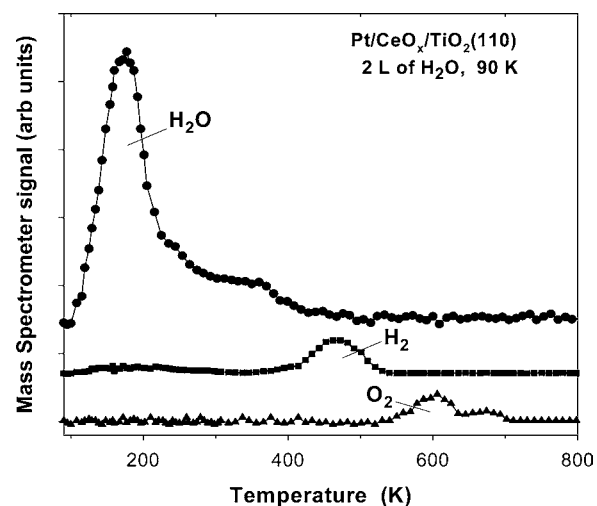


Figure 9. TPD spectra collected after dosing 2 langmuir of water onto a Pt/CeO_x/TiO₂(110) surface at ~ 90 K. The surface contained 0.2 ML of Pt, and $\sim 11\%$ of the titania was covered by ceria NPs.

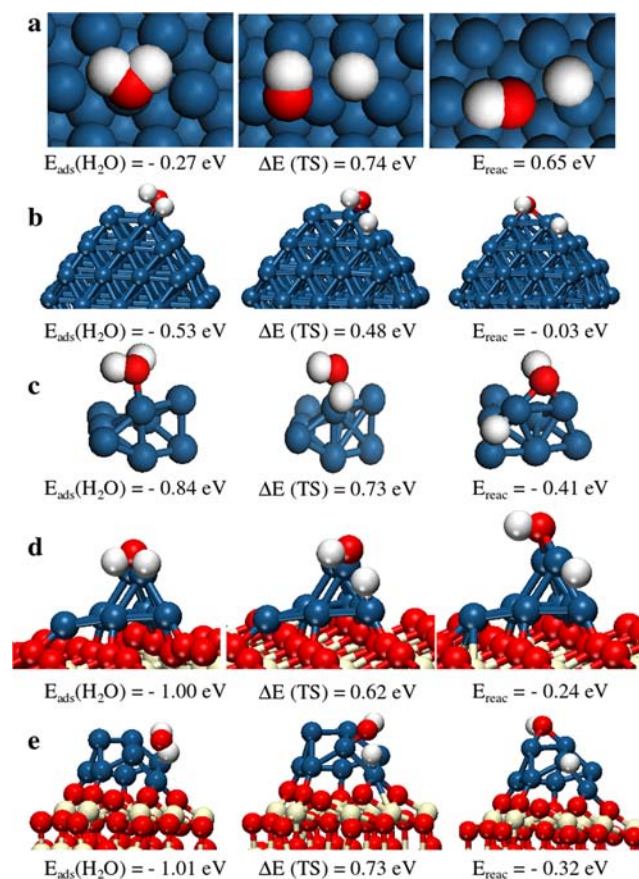


Figure 10. DFT-calculated structures for (left) adsorbed H₂O, (center) the transition state (TS), and (right) adsorbed HO + H along with the corresponding energy parameters [E_{ads} , $\Delta E(\text{TS})$, E_{rec}] for the dissociation of water over (a) a Pt(111) surface, (b) a free Pt₇₉ cluster, (c) a free Pt₈ cluster, and (d, e) Pt₈ clusters deposited on (d) a CeO₂(111) surface and (e) a Ce₄₀O₈₀ NP with a compact structure.²⁶ Pt, O, Ce, and H atoms are represented as blue, red, cream, and white spheres, respectively.

that of larger clusters.^{37,38} The Pt₇₉ and Pt₈ particles contain corner and edge atoms that have a coordination number significantly smaller than that of the atoms in a Pt(111)

surface.^{25,26} Pt₈ is highly fluxional and undergoes geometrical changes upon bonding of water or after interaction with CeO₂(111). The atoms of Pt₈ in contact with the CeO₂(111) surface (Figure 10d) or with the Ce₄₀O₈₀ NP (Figure 10e) are strongly bound to the oxygen sites of the oxide support with a net Pt → ceria charge transfer.^{25,26} The systems studied in Figure 10 allowed us to separate changes in reactivity due to variations in the coordination number of the Pt atoms [obtained by comparing the results for Pt(111) and Pt₇₉ or Pt₈] from changes in reactivity caused by the interaction of Pt with the ceria support [obtained by comparing the results for free Pt₈ and Pt₈ in contact with CeO₂(111) or the Ce₄₀O₈₀ NP].

Previous experimental³⁹ and theoretical studies^{7,15} indicated that Pt(111) has problems adsorbing and dissociating the water molecule and is not a good WGS catalyst.¹⁵ The dissociation of water on Pt(111) was calculated to be an endothermic process (Figure 11), in agreement with recent calorimetric measure-

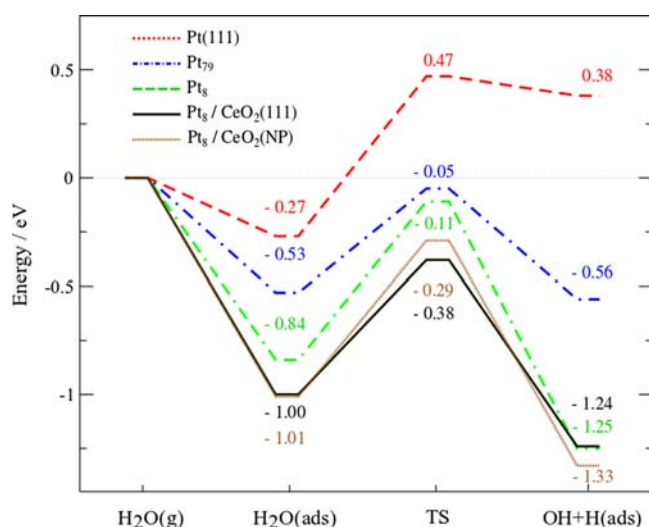


Figure 11. DFT-calculated energy profiles for the dissociation of water on Pt(111), Pt₇₉ and Pt₈ clusters, and Pt₈ on CeO₂(111) or a Ce₄₀O₈₀ NP. Figure 10 shows the calculated structures for the dissociation reaction.

ments.⁴⁰ The calculated exothermicity of the H₂O → H + OH reaction increased in going from Pt(111) to the free Pt₇₉ NP and even more in going to the free Pt₈ NP. The corner atoms present in the Pt₇₉ and Pt₈ NPs (Figure 10) facilitate cleavage of the O–H bonds, and a small particle like Pt₈ is more fluxional than Pt₇₉ in accommodating the reaction products (OH + H). These results indicate that the smaller the Pt particles, the easier the dissociation of water. This could explain the trends shown in Figures 2 and 8 for the variation of the WGS activity with Pt coverage. Furthermore, the DFT calculations showed an enhancement of the ability of Pt₈ to cleave O–H bonds when this cluster is deposited on a CeO₂(111) surface or on a Ce₄₀O₈₀ NP. For example, the adsorption of H₂O on Pt₈/CeO₂(111) leads to an energy release of ~1 eV that can be used to overcome the barrier for O–H bond cleavage. The resulting OH can react with CO, eventually yielding H₂ and CO₂ via the WGS reaction. The key to the chemical activity of Pt₈/CeO₂(111) lies in the electronic perturbations induced by ceria on Pt₈. Thus, the ceria-supported Pt₈ appears as a fluxional system that can change geometry and charge distribution to allow better accommoda-

tion of adsorbates. Compared with other WGS catalysts such as Cu/CeO₂(111) and Au/CeO₂(111),²⁰ the Pt/CeO₂(111) system has the unique property that the admetal is able to dissociate water in an efficient way. This is not the case for Cu/CeO₂(111) or Au/CeO₂(111), where water must dissociate on the oxide or at the oxide–metal interface.²⁰ Thus, small NPs of Pt in contact with CeO₂ can perform all the steps of the WGS reaction, making this system more active than Cu/CeO₂, Au/CeO₂, or Ni/CeO₂ (Figure 4). In addition, for Pt/CeO_x/TiO₂, the transfer of O from the ceria NPs to Pt (Figure 7 and ref 26) opens new paths that facilitate the dissociation of water on Pt (O_{ads} + H₂O → 2OH_{ads}),³⁹ and one could also easily move O produced by the dissociation of water on ceria²³ to Pt for subsequent reaction with CO. A generally accepted mechanism for the WGS reaction does not yet exist.^{5,6} Alternatives include associative mechanisms (i.e., formation of HCOO, HOCO, CO₃, or HCO₃ intermediates) and the redox mechanism.^{6–17} In any case, none of the traditional mechanisms takes into consideration a transfer of oxygen from the oxide support (ceria) to the admetal (Pt) that can affect the formation and stability of intermediates and be an important factor in the extremely high WGS activity of Pt/CeO_x/TiO₂.

In the literature of heterogeneous catalysis, it is well-known that the reactivity of the Pt/TiO₂ system can be affected by strong metal–support interactions.^{3,41} These interactions usually deactivate platinum and involve the decoration of the surface of the Pt particles with small aggregates of titania after reduction in H₂ at very high temperature (>770 K).⁴¹ This is completely different from the phenomena seen here, where admetal ↔ oxide electronic interactions significantly enhance the catalytic activity of Pt: Pt(111) ≪ Pt/CeO₂(111) < Pt/CeO_x/TiO₂(110). One must look for this type of interaction when designing metal/oxide catalysts that contain Pt. For example, we have found that the type of interaction that occurs on Pt/CeO₂ does not exist when Pt NPs are deposited on surfaces of alumina or silica. Thus, the Pt/Al₂O₃ and Pt/SiO₂ systems exhibit WGS activities that are 10–20 times smaller than that of Pt/CeO₂ and comparable to that of clean Pt(111).

SUMMARY AND CONCLUSIONS

The results of valence photoemission measurements and DFT calculations point to a new type of “strong metal–support interaction” for small Pt particles in contact with ceria. UPS spectra for the valence region of the Pt/CeO₂(111) and Pt/CeO_x/TiO₂(111) systems exhibited a density of Pt 5d states near the Fermi level that is much smaller than that expected for bulk metallic Pt. The Pt ↔ ceria interactions significantly enhance the ability of the admetal to adsorb water and dissociate the O–H bonds in the molecule. In going from Pt(111) to Pt₈/CeO₂(111), the dissociation of water becomes a very exothermic process (ΔE = −1.3 eV). Ceria-supported Pt₈ appears as a fluxional system that can change geometry and charge distribution to allow better accommodation of adsorbates such as H₂O, OH, and H. Compared with other WGS catalysts [Cu(111), Pt(111), Cu/CeO₂(111), and Au/CeO₂(111)], the Pt/CeO₂(111) surface has the unique property that the admetal is able to adsorb and dissociate water in an efficient way. XPS spectra taken after codeposition of Pt and CeO_x NPs on TiO₂(110) point to a transfer of O from the ceria to Pt that opens new paths for the WGS process and makes the mixed-metal oxide an extremely active catalyst for the production of hydrogen. In TPD experiments, the Pt/

CeO_x/TiO₂(110) surfaces were able to dissociate water fully into molecular H₂ and O₂.

AUTHOR INFORMATION

Corresponding Author

rodriguez@bnl.gov

Notes

The authors declare no competing financial interest.

ACKNOWLEDGMENTS

The work at BNL was financed by the U.S. Department of Energy (DOE), Office of Basic Energy Sciences, Chemical Sciences Division (DE-AC02-98CH10086). Calculations were carried out on the MARENOSTRUM supercomputer at the Barcelona Supercomputer Center. A.B. acknowledges the Spanish MICINN for a predoctoral grant. J.E. thanks INTEVEP and IDB for research grants that made possible part of this work at the Universidad Central de Venezuela.

REFERENCES

- (1) Campbell, C. T. *Surf. Sci. Rep.* **1997**, *27*, 1–111.
- (2) Farmer, J. A.; Campbell, C. T. *Science* **2010**, *329*, 933–936.
- (3) (a) Tauster, S. J.; Fung, S. C.; Garten, R. L. *J. Am. Chem. Soc.* **1978**, *100*, 170–175. (b) Tauster, S. J. *Acc. Chem. Res.* **1987**, *20*, 389–394.
- (4) (a) Diebold, U. *Surf. Sci. Rep.* **2003**, *48*, 53–229. (b) Pesty, F.; Steinrück, H.-P.; Madey, T. E. *Surf. Sci.* **1995**, *339*, 83–95.
- (5) Hinrichsen, K.-O.; Kochloefl, K.; Muhler, M. In *Handbook of Heterogeneous Catalysis*; Ertl, G., Knözinger, H., Schüth, F., Weitkamp, J., Eds.; Wiley-VCH: Weinheim, Germany, 2008.
- (6) Burch, R. *Phys. Chem. Chem. Phys.* **2006**, *8*, 5483–5495.
- (7) Zhai, Y.; Pierre, D.; Si, R.; Deng, W.; Ferrin, P.; Nilekar, A. U.; Peng, G.; Herron, J. A.; Bell, D. C.; Saltsburg, H.; Mavrikakis, M.; Flytzani-Stephanopoulos, M. *Science* **2010**, *329*, 1633–1636.
- (8) Jacobs, G.; Williams, L.; Graham, U.; Thomas, G. A.; Sparks, D. E.; Davis, B. H. *Appl. Catal., A* **2003**, *252*, 107–118.
- (9) Bunluesin, T.; Gorte, R. J.; Graham, G. W. *Appl. Catal., B* **1998**, *15*, 107–114.
- (10) Phatak, A. A.; Koryabkina, N.; Rai, S.; Ratts, J. L.; Ruettlinger, W.; Farruto, R. J.; Blau, G. E.; Delgass, W. N.; Ribeiro, F. H. *Catal. Today* **2007**, *123*, 224–234.
- (11) Lida, H.; Kondo, K.; Igarashi, A. *Catal. Commun.* **2006**, *7*, 240–244.
- (12) Panagiotopoulou, P.; Christodoulakis, A.; Kondarides, D. I.; Boghosian, S. J. *Catal.* **2006**, *240*, 114–125.
- (13) Kalamaras, C. M.; Gonzalez, I. D.; Navarro, R. M.; Fierro, J. L. G.; Efstathiou, A. M. *J. Phys. Chem. C* **2011**, *115*, 11595–11610.
- (14) Gonzalez, I. D.; Navarro, R. M.; Wen, W.; Marinkovic, N.; Rodriguez, J. A.; Rosa, F.; Fierro, J. L. G. *Catal. Today* **2010**, *149*, 372–379.
- (15) Flaherty, D. W.; Yu, W.-Y.; Pozun, Z. D.; Henkelman, G.; Mullins, C. B. *J. Catal.* **2011**, *282*, 278–288.
- (16) Nakamura, J.; Campbell, J. M.; Campbell, C. T. *J. Chem. Soc., Faraday Trans.* **1990**, *86*, 2725–2730.
- (17) Gokhale, A. A.; Dumesic, J. A.; Mavrikakis, M. *J. Am. Chem. Soc.* **2008**, *130*, 1402–1414.
- (18) Rodriguez, J. A.; Graciani, J.; Evans, J.; Park, J. B.; Yang, F.; Stacchiola, D.; Senanayake, S. D.; Ma, S.; Perez, M.; Liu, P.; Sanz, J. F.; Hrbek, J. *Angew. Chem., Int. Ed.* **2009**, *48*, 8047–8050.
- (19) Park, J. B.; Graciani, J.; Evans, J.; Stacchiola, D.; Ma, S.; Liu, P.; Nambu, A.; Sanz, J. F.; Hrbek, J.; Rodriguez, J. A. *Proc. Natl. Acad. Sci. U.S.A.* **2009**, *106*, 4975–4980.
- (20) Rodriguez, J. A.; Liu, P.; Hrbek, J.; Evans, J.; Perez, M. *Angew. Chem., Int. Ed.* **2007**, *46*, 1329–1332.
- (21) Mullins, D. R.; Radulovic, P. V.; Overbury, S. V. *Surf. Sci.* **1999**, *429*, 186–194.
- (22) Lu, J. L.; Gao, H. J.; Shaikhtudinov, S. K.; Freund, H. J. *Catal. Lett.* **2007**, *114*, 8–16.
- (23) Park, J. B.; Graciani, J.; Evans, J.; Stacchiola, D.; Senanayake, S. D.; Barrio, L.; Liu, P.; Sanz, J. F.; Hrbek, J.; Rodriguez, J. A. *J. Am. Chem. Soc.* **2010**, *132*, 356–363.
- (24) Kresse, G.; Hafner, J. *Phys. Rev. B* **1993**, *47*, 558–561.
- (25) Bruix, A.; Migani, A.; Vayssilov, G. N.; Neyman, K. M.; Libuda, J.; Illas, F. *Phys. Chem. Chem. Phys.* **2011**, *13*, 11384–11392.
- (26) Vayssilov, G. N.; Lykhach, Y.; Migani, A.; Staud, T.; Petroval, G. P.; Tsud, N.; Skála, T.; Bruix, A.; Illas, F.; Prince, K. C.; Matolín, V.; Neyman, K. M.; Libuda, J. *Nat. Mater.* **2011**, *10*, 310–315.
- (27) Migani, A.; Vayssilov, G. N.; Bromley, S. T.; Illas, F.; Neyman, K. M. *Chem. Commun.* **2010**, *46*, 5936–5938.
- (28) Loschen, C.; Carrasco, J.; Neyman, K. M.; Illas, F. *Phys. Rev. B* **2007**, *75*, No. 035115.
- (29) Zhou, Y.; Perket, J.; Zhou, J. *J. Phys. Chem. C* **2010**, *114*, 11853.
- (30) (a) Paffett, M. T.; Gebhard, S. C.; Windham, R. G.; Koel, B. J. *Phys. Chem.* **1990**, *94*, 6831–6839. (b) Pirug, G.; Bonzel, H. P.; Broden, G. *Surf. Sci.* **1982**, *122*, 1–20.
- (31) Senanayake, S. D.; Evans, J.; Agnoli, S.; Barrio, L.; Chen, T.-L.; Hrbek, J.; Rodriguez, J. A. *Top. Catal.* **2011**, *54*, 34–41.
- (32) Park, J. B.; Conner, S. F.; Chen, D. A. *J. Phys. Chem. C* **2008**, *112*, 5490–5500.
- (33) Larese, C.; Cabello Galisteo, F.; Lopez Granados, M.; Mariscal, R.; Fierro, J. L. G.; Lambrou, P. S.; Efstathiou, A. M. *J. Catal.* **2004**, *226*, 443–456.
- (34) Parkinson, C. R.; Walker, M.; McConville, C. F. *Surf. Sci.* **2003**, *545*, 19–33.
- (35) Zehr, R. T.; Henderson, M. A. *Surf. Sci.* **2008**, *602*, 1507–1516.
- (36) Clay, C.; Haq, S.; Hodgson, A. *Phys. Rev. Lett.* **2004**, *92*, No. 046102.
- (37) Vajda, S.; Winans, R. E.; Elam, J. W.; Lee, B.; Pellin, M. J.; Seifert, S.; Tikhonov, G. Y.; Tomczyk, N. A. *Top. Catal.* **2006**, *39*, 161–166.
- (38) Heiz, U.; Sanchez, A.; Abbet, S.; Schneider, W.-D. *Chem. Phys.* **2000**, *262*, 189–200.
- (39) (a) Fischer, G. B.; Sexton, B. A. *Phys. Rev. Lett.* **1980**, *44*, 683–686. (b) Bedürftig, K.; Volkening, S.; Wang, Y.; Wintterlin, J.; Jacobi, K.; Ertl, G. *J. Chem. Phys.* **1999**, *111*, 11147–11154.
- (40) Lew, W.; Crowe, M. C.; Karp, E.; Lytken, O.; Farmer, J. A.; Arnadottir, L.; Schoenbaum, C.; Campbell, C. T. *J. Phys. Chem. C* **2011**, *115*, 11586–11594.
- (41) Datye, A. K.; Kalakkad, D. S.; Yao, M. H.; Smith, D. J. *J. Catal.* **1995**, *155*, 148–153.